

1 **Sampling method for the determination of methane emissions from landfill**
2 **surfaces**

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11 **Abstract**

12 The first aim of this work is the definition and the study of a suitable sampling method for the
13 measurement of landfill gas (LFG) emissions from landfill surfaces, since, up to now, there are no
14 codified nor universally accepted sampling methods for this specific task. The studied sampling method
15 is based on the use of a static hood. The research work involves a preliminary theoretical study for the
16 hood design, experimental tests for the definition of the optimal sampling procedures, and simulations of
17 the hood fluid-dynamics for the system validation. The second aim of this study is the investigation of the
18 correlations between LFG emissions and meteorological conditions, whose identification would be very
19 useful in terms of effective landfill management and pollution control. This involved a wide literature
20 study for the selection of those parameters that seem to have an influence on LFG emission, and the
21 collection of a great number of experimental data on a target site, which led to the conclusion that
22 atmospheric pressure and soil humidity are the parameters that mostly affect LFG emissions.

23 **Keywords:** landfill, sampling, passive area sources, static hood, flux chamber, CFD, surface emissions.

24 **Introduction**

25 Landfills are significant sources of pollution (Kumar *et al.*, 2004). Disposal of waste in such sites leads to
26 the generation of a leachate, which may pollute the land and the aquifer (Renou *et al.*, 2008), and a
27 biogas, a mixture of carbon dioxide (CO₂) and methane (CH₄), greenhouse gases and pollutants (Young &
28 Parker, 1983). Landfills are typically also an important source of odour pollution (Palmiotto *et al.*, 2014),
29 because of the presence in landfill biogas (LFG) of traces of compounds characterized by very low odour
30 detection thresholds (Davoli *et al.*, 2003; Capelli *et al.*, 2008), giving that LFG emissions can be related
31 to odour emissions from a landfill (Lucernoni *et al.*, 2016a).

32 Even though modern landfills are always equipped with a gas capture system, a portion of the gas escapes
33 and is emitted into the atmosphere through the surface. Thus, the possibility of quantifying the LFG
34 surface emissions and monitoring them over time may represent an important aspect for the landfill
35 operation and management (Mosher *et al.*, 1999). Quantification of LFG emissions, and their possible
36 correlation to odour emissions, requires the periodical execution of specific measurement campaigns,
37 which should be carried out by means of a suitable sampling method that should be repeatable,
38 reproducible and accurate. This is a complicated task: to date, there are no codified nor universally
39 accepted sampling methods.

40 Despite in literature several studies hypothesize the existence of some sort of correlations between
41 meteorological conditions and emissions, such correlations are undemonstrated, mostly contrasting, and
42 never quantified. For this reason, it is not known how to account for the effect of the changing
43 meteorological conditions on the LFG emissions.

44 The first aim of this work is the definition of a sampling method that allows for reproducible and
45 repeatable measurements. As already mentioned, to date the best way for LFG sampling on landfill
46 surfaces is still debated in the scientific community.

47 On a regulatory level, there are two different approaches, both based on so called “hood methods”,
48 involving the use of a specific sampling hood that isolates a portion of the surface to be sampled. The
49 oldest – and more consolidated – is the EPA method (EPA, 1986), which entails the use of a flux chamber
50 (FC) flushed with a neutral gas flow (N₂ or air) (Reinhart *et al.*, 1992; Park & Shin, 2001; Gebert *et al.*,
51 2011; Di Trapani *et al.*, 2013). The other one, adopted by the UK-EA (EA, 2010), entails the use of a
52 static hood (SH), in which the increase of methane concentration is measured over time. The static
53 chamber measurement approach, for methane and LFG emission determination from landfill surfaces, is
54 the most often used in Italy and it is also commonly applied in many cases outside of the UK because it is
55 relatively inexpensive, simple, and highly sensitive at detecting even small fluxes (Abichou *et al.*, 2006;
56 Bogner *et al.*, 1995; Cardellini *et al.*, 2003; Schroth *et al.*, 2012); thus new and optimized designs for
57 static chambers have been recently proposed (Rachor *et al.*, 2013; Lucernoni *et al.*, 2016b).

58 Moreover, hood methods, and especially fluxed hoods, are by far the preferred method for the assessment
59 of odour emissions from passive area sources (Hudson & Ayoko, 2008; Capelli *et al.*, 2013; Parker *et al.*,
60 2013), and also from landfill surfaces (Sarkar & Hobbs, 2002; Frechen *et al.*, 2004; Sironi *et al.*, 2005;
61 Romain *et al.*, 2008).

62 However, as far as the assessment of CH₄ and LFG emissions from landfills are concerned, several
63 alternatives to hood sampling methodologies exist, which are worth to be mentioned.

64 • The main alternative is the tracer gas (TG) method entailing the controlled release on the
65 emission surface of a given traceable gas (*e.g.* SF₆), used to simulate the landfill gaseous
66 emissions (Börjesson *et al.*, 2000; Spokas *et al.*, 2003). There are different options depending on
67 the tracer gas used and on the kind of measurement performed. The main two possibilities are
68 mobile or static measurement. The mobile plume measurement (MPM) consists in driving with a
69 tuneable diode laser spectrometer (TDL) along a downwind transect perpendicular to the wind
70 direction around 200 m from the site to measure tracer gas concentrations in the plume’s cross

71 section. An inlet tube is located at the front of the van above the cabin to let the outside air come
72 into the TDL system; this avoids additional mixing. A tracer gas (*e.g.* N₂O) is released with a
73 known constant flow-rate from the source and used as a reference compound to calibrate the
74 model. The released gas flow is controlled; before and after the experiments the tracer bottles are
75 weighted to know the exact volume of tracer gas lost within the release period. The emission is
76 calculated from the measured/modelled concentration levels above the background (Babilotte *et*
77 *al.*, 2010). The static plume measurement (SPM) entails using vacuum gas bottles installed at a
78 road downwind of the source. The bottles are evacuated before the measurements with a vacuum
79 pump and will fill themselves to approximately 0.5 bar, requiring a defined time. After, the
80 bottles are closed and analysed with a TDL system. One of the bottles is used for the assessment
81 of the background concentration of CH₄ and tracer gas; this one needs to be located upwind of
82 the landfill. The emission from the source is calculated from the measured/modelled
83 concentration levels above the background (Simpson *et al.*, 1995; Babilotte *et al.*, 2010).

- 84 • The radial plume mapping (RPM) entails the use of optical remote sensing (ORS) for the
85 collection of path-integrated concentration (PIC) data over multiple, non-overlapping beam paths
86 (Babilotte *et al.*, 2010).
- 87 • The differential absorption LiDAR – or Light Detection And Ranging - (DiAL) technique is a
88 laser-based remote monitoring, enabling range-resolved concentration measures of a large
89 variety of atmospheric chemical compounds both in the infra-red (*e.g.* CH₄, C₂H₆, etc.) and
90 ultra-violet wave-length spectrum (*e.g.* NO_x, SO_x, etc.) with a ppm sensitivity at ranges higher
91 than 500 m. The system consists of an accessorized self-powered truck. In the DiAL, the laser is
92 operated alternately at two adjacent wavelengths. The on-resonant wavelength is chosen to be at
93 a wavelength that is absorbed by the target species. The off-resonant wavelength is chosen to be
94 at a wavelength that is not absorbed by the target species in order to avoid interferences.

95 Emission fluxes are measured scanning the DiAL measurement beam in a vertical plane
96 downwind of the target sources and determining the total concentration of CH₄ above the
97 background in that plane. Vertical planes are typically 600 m x 600 m with a range resolution of
98 25 m vertically and 5 m horizontally. To determine the emission flux of CH₄ due to the landfill
99 site itself, the background CH₄ needs to be subtracted from the concentration profiles before the
100 flux is calculated (Babilotte *et al.*, 2010).

101 • The inverse modelling (IM) entails the use of a concentration analyser that provides real-time
102 CH₄ concentration measures. Concentration measures are performed at discrete receptors
103 downwind of the landfill. CH₄ concentrations and associated Global Positioning System (GPS)
104 coordinates are then used in an atmospheric dispersion modelling software (*e.g.* ADMS3,
105 CALPUFF, etc.). The software performs an inverse modelling analysis according to the geo-
106 referenced CH₄ concentrations. The output is a CH₄ emission factor for each landfill cell
107 (Babilotte *et al.*, 2010).

108 As previously mentioned, there are several literature works describing the possibility to use hood methods
109 for measuring both LFG (Reinhart *et al.*, 1992; Bogner *et al.*, 1995; Park & Shin, 2001; Cardellini *et al.*,
110 2003; Abichou *et al.*, 2006; Gebert *et al.*, 2011; Schroth *et al.*, 2012; Di Trapani *et al.*, 2013; Liu *et al.*,
111 2015) and odour (Sarkar & Hobbs, 2002; Frechen *et al.*, 2004; Sironi *et al.*, 2005; Romain *et al.*, 2008)
112 emissions from landfills. As demonstrated in other previous works, odour emissions from landfill surfaces
113 can be determined either by means of direct odour sampling, or indirectly, *i.e.* by measuring the LFG
114 emissions and then multiplying the LFG flux by the LFG odour concentration (Lucernoni *et al.*, 2016a,
115 2017). In this second case, the odour concentration of the LFG emitted through the landfill surface needs
116 to be estimated by relating the CH₄ and the odour concentration of samples collected over the landfill
117 surface (Lucernoni *et al.*, 2016a, 2017). Even though odour measurement is not the primary objective of
118 this work, because of the above mentioned possibility to relate CH₄ and odour concentration data, hood

119 methods were preferred as the investigated method for the development of a sampling methodology that
120 allows both the measurement of LFG fluxes and of odour emissions.

121 The development of the sampling methodology involved: a preliminary theoretical study for the hood
122 design, experimental tests for the definition of optimal sampling procedures and operative conditions and
123 a fluid-dynamic study exploiting computational fluid dynamics (CFD) simulations for the system
124 validation.

125 The second goal of the study is the investigation of the correlations between LFG emissions and
126 meteorological parameters. This involved a wide literature study for the selection of those parameters that
127 seem to have an influence on the LFG emission. The identification of such a correlation would be useful
128 in terms of effective landfill management and pollution control.

129 **Materials and methods**

130 *Experimental campaigns*

131 The site is a landfill in Northern Italy operative since 1993, it has an extension of 250 000 m² subdivided
132 in 6 allotments of which only one still is operational. The landfill waste storage capacity amounts to
133 roughly 6 200 000 m³. The LFG collection system sucks 2200 m³ h⁻¹ of gas, which is burnt in four co-
134 generators for the production of electric energy. The campaigns were planned with a frequency of two
135 times per week on average, for a total of 40: from December 2014 to November 2015 in allotments 1 and
136 2, both closed and covered with a clay layer, without waterproofing seal. Four different points were
137 identified for LFG sampling from December 2014 to March 2015, since two of these points resulted
138 scarcely emissive (not measurable), these points were discarded and replaced with three new points for
139 the measurements from March 2015 to November 2015. Measures were carried out always at the same
140 time, around 11 a.m., in order to prevent additional variability.

141 *Materials*

142 The device developed at the Politecnico di Milano for CH₄ sampling over landfill surfaces is a hood (Fig.
143 1), which was designed based on the one described in the UK-EA (EA, 2010) and by the modified version
144 proposed by Rachor *et al.* (2013). The hood has a squared base, 50 cm x 50 cm, with a height of 10 cm
145 and it is connected to the outside by means of a 3 m long Teflon tube that allows keeping the internal
146 pressure equal to the atmospheric pressure in order to avoid over-pressures that may affect the emission.
147 The device is made of steel. A 10 cm long tube on the top of the hood allows the CH₄ concentration
148 measurement by attaching a Flame Ionization Detector (FID), which has a suction flow of 1.06 l min⁻¹, to
149 the outlet tube for 2 min. The CH₄ concentration analyser used is a Crowcon GasTec portable FID, with a
150 detection range of 0-10000 ppm and an accuracy of 1 ppm.



151
152 **Figure 1.** *The sampling hood designed at the Politecnico di Milano operated as a FC (left) and as a SH*
153 *(right).*

154 One particular feature of this newly designed hood is that it can be operated both as a FC or as a SH, i.e.
155 with or without the introduction of a neutral sweep air flow, respectively. This gives the advantage of
156 allowing both the direct and indirect measurement of odour emissions from landfill area sources. Direct
157 odour measurement needs to be performed using the hood as a FC, since the withdrawal of the

158 olfactometric sample volume would perturb the internal SH too much; this is less true for a FC whose
 159 internal volume is continuously flushed by a neutral gas flow. On the other hand, indirect odour emission
 160 measurement can be carried out with both hoods, since this method relies primarily on the evaluation of
 161 the LFG flux through the measurement of the CH₄ concentration over the landfill surface, and the
 162 subsequent estimation of the odour emission rate by multiplication with the LFG odour concentration
 163 (Lucernoni *et al.*, 2016a, 2017).

164 In order to evaluate the possibility to use the designed hood in both modes (fluxed or static), in the period
 165 from December to March the hood was operated both as a FC and a SH to compare the two sampling
 166 methods.

167 The procedure defined for the FC mode (Fig. 1, left) provides that the hood is fluxed with a neutral air
 168 flow of 200 l h⁻¹ for a period of 12 min by connecting an air bottle to the tube on the top of the hood.

169 The SH mode procedure provides that the hood is positioned on the landfill surface for a period of 10 min
 170 before measuring the CH₄ concentration. From the CH₄ concentration, it is possible to calculate the
 171 specific emissive LFG flow, in l m⁻² h⁻¹. The presence of the lateral tube connecting the interior of the
 172 hood with the external ambient assuring isobaric conditions during sampling also guarantees that a higher
 173 CH₄ concentration inside the hood is avoided without continuously sweeping the air out of the hood
 174 (Rachor *et al.*, 2013; Lucernoni *et al.*, 2016b).

175 For the fluxed mode, it is possible to write the CH₄ mass balance as:

$$176 \quad \dot{Q}_{out} \cdot c_{CH_4,mis} = \dot{Q}_{in} \cdot c_{CH_4,in} + \dot{Q}_{LFG} \cdot c_{CH_4,LFG} \quad (1)$$

177 In Eq.1 (\dot{Q}_{out}) is the total flow [l h⁻¹] equal to the inlet air flow ($\dot{Q}_{in} = 200 \text{ l h}^{-1}$) plus the emitted LFG
 178 flow (\dot{Q}_{LFG}), ($c_{CH_4,mis}$) is the measured CH₄ concentration [$\mu\text{mol mol}^{-1}$], ($c_{CH_4,in}$) is the CH₄
 179 concentration in the neutral air equal to zero [$\mu\text{mol mol}^{-1}$] and ($c_{CH_4,LFG}$) is the concentration in the pure
 180 LFG equal to 500 000 [$\mu\text{mol mol}^{-1}$], that is 50% molar fraction. The CH₄ concentration of 50% in the
 181 pure LFG is a datum obtained from the operational information regarding the LFG collection and

182 combustion system of the landfill. Since the emitted LFG flow rate is much lower than the fluxed neutral
 183 air, it is possible to assume that (\dot{Q}_{out}) and (\dot{Q}_{in}) are equal. The specific LFG flow (\hat{Q}_{LFG}) [$l\ m^{-2}\ h^{-1}$] is
 184 obtained by dividing by the base area of the hood (S_h), which is $0.25\ m^2$:

$$185 \quad \hat{Q}_{LFG} = \frac{Q_{in} \cdot c_{CH_4, mis}}{c_{CH_4, LFG} \cdot S_h} \quad (2)$$

186 When operating the hood as a SH (Fig. 1, right), it is possible to write the mass balance for CH_4 as
 187 shown:

$$188 \quad V \cdot \frac{d\bar{c}_{CH_4}}{dt} = \dot{Q}_{LFG} \cdot c_{CH_4, LFG} \quad (3)$$

189 In Eq. 3, (V) is the volume of the hood equal to $25\ [l]$, $(\frac{d\bar{c}_{CH_4}}{dt})$ is the average CH_4 concentration variation
 190 inside the hood over time, (\dot{Q}_{LFG}) is the emitted LFG flow [$l\ h^{-1}$] and $(c_{CH_4, LFG})$ is the concentration in
 191 the pure LFG equal to $500\ 000\ [\mu mol\ mol^{-1}]$. The specific LFG flow may be obtained by making two
 192 assumptions:

- 193 I. the CH_4 concentration inside the hood has a linear growth over time;
- 194 II. the CH_4 concentration that is measured by means of the FID is equal to the average CH_4
 195 concentration inside the hood \bar{c}_{CH_4} .

196 The specific LFG flow can be computed by using Eq.4:

$$197 \quad \hat{Q}_{LFG} = \frac{c_{CH_4, mis} \cdot V}{c_{CH_4, LFG} \cdot \Delta t \cdot S_h} \quad (4)$$

198 *CFD simulations*

199 Computational Fluid Dynamics (CFD) was applied to study the static sampling procedure, since the
 200 understanding of the fluid-dynamic behaviour of the sampling hood is fundamental for the correct
 201 interpretation of the sampled data (Prata Jr. *et al.*, 2016). CFD simulations with the software ANSYS
 202 Fluent were performed with the aim of verifying the assumptions of linear growth of the CH_4
 203 concentration inside the hood and of equivalence of measured CH_4 concentration and average CH_4

204 concentration inside the hood, on which the method (Eq.4) is based. This fluid-dynamic study is
205 fundamental to verify the appropriateness of the developed sampling method, thereby involving the
206 verification of the pertinence of the choice of the sampling point and of the sampling time, thus proving
207 the representativeness of the adopted procedure for the determination of the emitted LFG flow rate. The
208 advantage of this approach is to avoid the perturbation in the concentration inside the chamber induced by
209 the flow of the FID, which would make it very difficult experimentally to evaluate the concentration in a
210 precise point and impossible during a single test.

211 In order to apply CFD, it was first necessary to generate a suitable mesh that provides the software with a
212 discrete representation of the hood geometry. The adopted mesh is non-structured with a refinement of 14
213 layers of structured mesh at the inlet boundary (as shown in Fig. 4) and a total number of cells of 3 000
214 000. Then the simulation settings have to be defined: the source term was set equal to $0.25 [l m^{-2} h^{-1}]$,
215 which is the mean specific LFG flow emitted from the landfill surface, deriving from the experimental
216 campaigns on site. This value is not the final datum, but it is a value obtained during the first campaigns,
217 in order to perform the CFD study assessing the appropriateness of the adopted sampling method in the
218 early stages of the project. The model also requires setting the values of pressure, temperature, and
219 diffusivity coefficients. The simulations were run considering a total time of 12 min: 10 min of static
220 hood positioning + 2 min for the FID analysis.

221 *Correlation between meteorological data and LFG emissions*

222 In order to investigate the existence of a correlation between LFG emissions from the landfill surface and
223 meteorological conditions, a great number of emission and meteorological data are required. Before
224 starting the analysis of the experimental data acquired from the measurement campaigns on site, a
225 thorough review of the scientific literature on the subject was performed to identify the meteorological
226 parameters that other authors had investigated as possibly affecting the LFG emissions. As a first result of
227 this first literature review step, Tab. 1 tries to resume a bibliographic overview of what has been written

228 by other researchers on this matter by summarizing their statements and observations about the influence
 229 of atmospheric parameters on LFG emissions.

230 Finally, the meteorological data considered for the study were rainfall, temperature, atmospheric pressure,
 231 wind speed, relative humidity and solar radiation. In addition, the soil humidity was considered as well,
 232 which was determined experimentally by collecting soil samples and weighting them before and after
 233 drying, thus assessing the humidity as the removed water fraction.

234 **Table 1.** *Bibliographic overview of the statements and observations about the influence of atmospheric*
 235 *parameters on LFG emissions made by other researchers.*

Atmospheric Parameter	Source(s)	Correlation Type	Author's Hypothesis
Atmospheric Pressure (P)	Reinhart <i>et al.</i> , 1992; McBain <i>et al.</i> , 2005	<u>Negative Correlation (-):</u> P increases and LFG flow decreases	Landfill "respiration"
Temperature (T)	Park & Shin, 2001	<u>Positive Correlation (+):</u> T increases and LFG flow increases	Waste decomposition process is enhanced
Temperature (T)	Rachor <i>et al.</i> , 2013	<u>Negative Correlation (-):</u> T increases and LFG flow decreases	Temperature governs microbial CH ₄ oxidation because chemical processes in the cells are faster at greater energy supplies (i.e during the warm season)
Soil Humidity (U)	Rachor <i>et al.</i> , 2013	<u>Positive Correlation (+):</u> U increases and LFG	CH ₄ production is enhanced in a moist environment and CH ₄

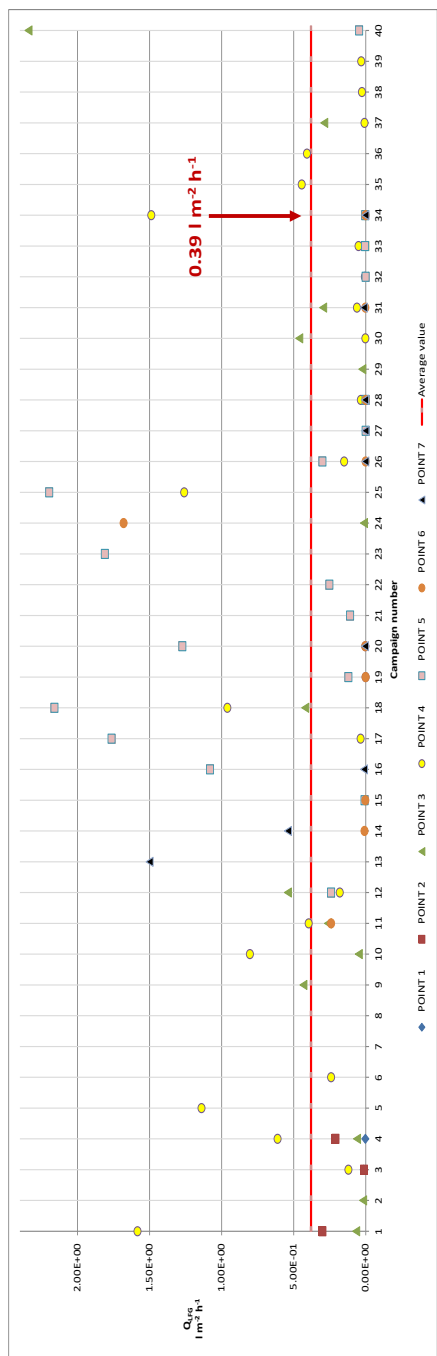
		flow increases	oxidation is disadvantaged by lack of O ₂ (pores occupied by H ₂ O)
Soil Humidity (U)	Rachor <i>et al.</i> , 2013	<u>Negative Correlation (-):</u> U increases and LFG flow decreases	CH ₄ oxidation is favoured, more favourable environment for metanotroph bacteria
Wind Velocity (v)	McBain <i>et al.</i> , 2005	<u>Positive Correlation (+):</u> v increases and LFG flow increases	Diffusive resistance is lowered, the boundary layer thickness decreases
Wind Velocity (v)	Rachor <i>et al.</i> , 2013; Reinhart <i>et al.</i> , 1992	<u>Negative Correlation (-):</u> v increases and LFG flow decreases	Wind velocity influences the pressure value on soil surface, P increases
Rainfalls (p)	Rachor <i>et al.</i> , 2013	<u>Negative Correlation (-):</u> p increases and LFG flow decreases	Cork effect, water prevents LFG from going into the atmosphere

236 Results and discussion

237 *Definition of the sampling method*

238 Fig. 2 shows LFG specific flow data obtained in the different sampling points for all experimental
 239 campaigns. In order to define the most suitable sampling method, emission data obtained with the SH
 240 have been compared with those obtained with the FC until March: the comparison showed no dramatic
 241 differences between the two methods (Fig. 3).

242



243

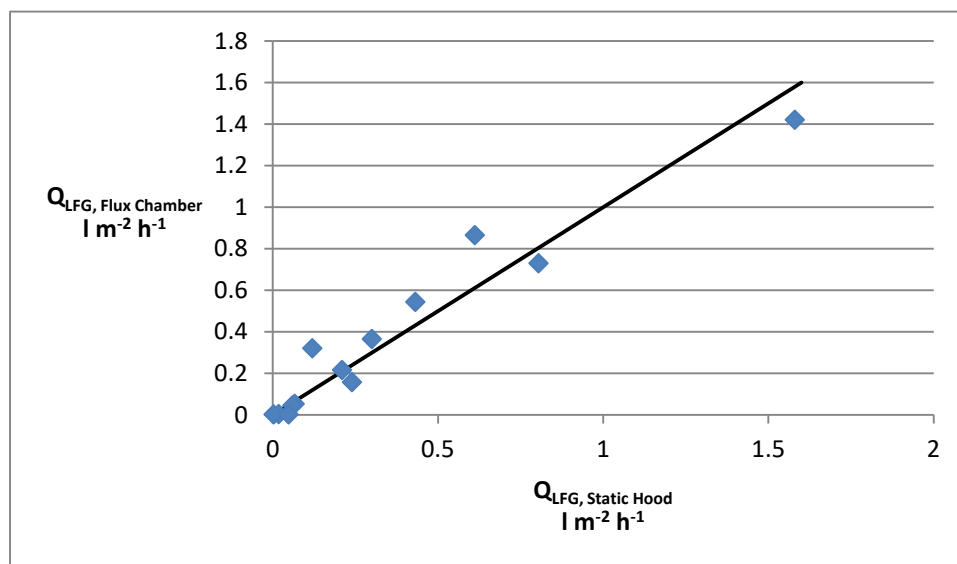
244

Figure 2. Results of the experimental campaigns (specific LFG flow rates in $l\ m^{-2}\ h^{-1}$).

245 The average flux highlighted in Fig. 2 is obtained computing the arithmetic mean, in accordance with the
 246 criteria in the guideline of the UK Environment Agency (UK-EA, 2010).

247 The mean specific LFG flux value turned out to be $0.39 \text{ l m}^{-2} \text{ h}^{-1}$. There is a significant variability of the
 248 experimental data (Fig. 2), which is the case in environmental measurement campaigns, since the
 249 measurement is highly affected by different factors. In Fig. 2, the majority of the flux values are rather
 250 low while the high ones represent a smaller share. The method adopted to assess the LFG flux has been
 251 used in a recent publication to assess odour emissions from landfill surfaces (Lucernoni *et al.*, 2016a).

252 By plotting the LFG flux data (Fig. 3) with the SH data on the x-axis and the FC data on the y-axis, it is
 253 possible to see how the resulting points are very close to the line representing perfect equivalence
 254 between the two methods (*i.e.* $x=y$). Once verified that both methods provide similar results in terms of
 255 CH_4 – and thus also in terms of related odour – emission fluxes, it was decided to prefer the SH method,
 256 since it is less demanding especially as far as logistics is concerned, as it does not involve the need to
 257 provide a neutral sweep air flow (*i.e.* no need to transport and consume air bottles, or to use a rotameter).



258

259 **Figure 3.** Comparison between LFG emission data obtained with FC and SH ‘

260

(December 2014 – March 2015).

261 The mean specific LFG flow rate derived from the experimental measurements turned out to be equal to
262 $0.39 \text{ l m}^{-2} \text{ h}^{-1}$. This value is similar to that found in literature in a study by Palmiotto *et al.* (2014), in a
263 MSW landfill located also in Northern Italy, which is likely to have both landfilled waste quality and
264 landfill management operations similar to those of the landfill considered for this study. In that case, the
265 obtained surface LFG flux is equal to $0.2 \text{ l m}^{-2} \text{ h}^{-1}$ (Palmiotto *et al.*, 2014). In parallel, a CFD simulation
266 of the sampling with the hood was performed to see if the sampling system adopted was proper for the
267 study.

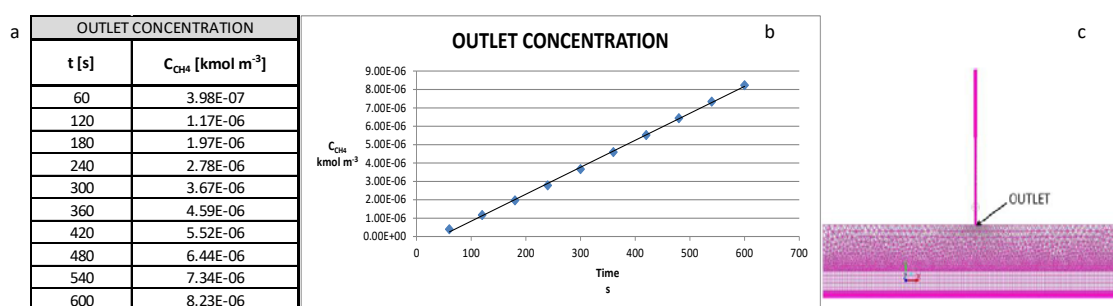
268 *CFD simulation of the sampling procedure with SH*

269 In order to verify the assumptions of linear growth of the CH_4 concentration inside the SH and of
270 equivalence of measured CH_4 concentration and average CH_4 concentration inside the hood, which the
271 adopted sampling method relies on, it was decided to evaluate the CH_4 concentration at some specific
272 points inside the hood with a CFD simulation. The LFG specific flux imposed as source term for the CFD
273 simulations is not $0.39 \text{ l m}^{-2} \text{ h}^{-1}$, as finally resulting from the experimental campaigns, but $0.25 \text{ l m}^{-2} \text{ h}^{-1}$.
274 This discrepancy is because it was necessary to run the preliminary simulations by means of CFD to
275 describe the fluid-dynamic behaviour of the hood before completing the experimental campaigns in the
276 field to validate the sampling system. For this reason, the specific LFG flux of $0.25 \text{ l m}^{-2} \text{ h}^{-1}$ used for the
277 simulations is a partial result that was obtained after the first campaigns. The fact that the “true” value
278 resulting after completion of the experimental data collection turned out to be $0.39 \text{ l m}^{-2} \text{ h}^{-1}$, does not
279 affect the significance and validity of the CFD simulations, since the two values do not differ
280 substantially. In order to confirm this assumptions other simulations were run subsequently changing the
281 LFG specific flux in a range from $0.05 \text{ l m}^{-2} \text{ h}^{-1}$ to $1 \text{ l m}^{-2} \text{ h}^{-1}$, as described in the paper by Lucernoni *et al.*
282 (2016b).

283 Fig. 4 shows the results of the simulation relevant to the point at the outlet orifice on top of the hood,
284 where the shorter tube is attached and where the FID is inserted for the concentration measurement. The

285 values at each minute from 0 to 10 in kmol m^{-3} and the resulting plot over time are reported. It is possible
 286 to observe that the concentration points are linearly interpolated, with a correlation index R^2 of 0.9991,
 287 confirming the first hypothesis of linear increase of the CH_4 concentration inside the hood. This linear
 288 growth for short horizon times is observed for all the points on the central axis of the hood.

289



290

291 **Figure 4.** Methane concentration values over time (a), concentration trend over time at the hood outlet
 292 (b) and mesh representation for the device highlighting the outlet (c).

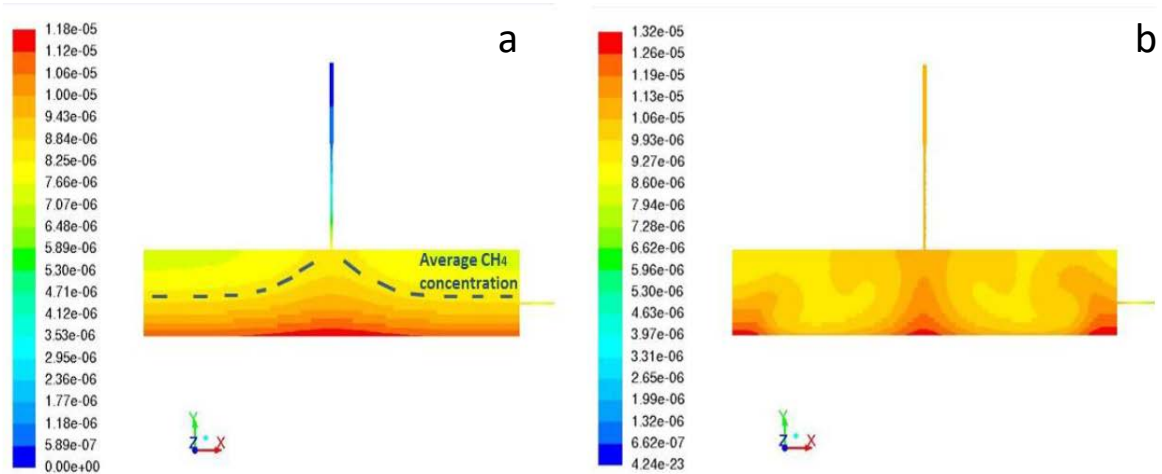
293 The CFD simulation also allowed to verify the second assumption - that the CH_4 concentration read by
 294 the FID is representative of the average CH_4 concentration inside the hood - by analysing the CH_4
 295 concentration contours inside the hood over time, i.e. during the first 10 min in which the SH is
 296 positioned over the landfill surface and during the following 2 min of the FID measurement duration.

297 The LFG flow rate considered as source term (i.e. $0.25 \text{ l m}^{-2} \text{ h}^{-1}$) is rather low, so no mixing is foreseen
 298 inside the hood; this was confirmed by the simulation showing that the CH_4 concentration distribution
 299 inside the SH after 10 min is not homogeneous, but stratified (Fig. 5a). The simulation results sketched in
 300 Fig. 5a show also that the stratification is bell shaped, the typical concentration distribution in case of
 301 plug flow with axial diffusion: this is corroborated by the order of magnitude of the diffusive velocity, 10^{-4}
 302 m s^{-1} , higher than the convective velocity inside the hood, order of magnitude of 10^{-7} m s^{-1} . Thus, after
 303 the established “deposition” time of 10 min, the CH_4 concentration at the sampling point (the outlet), is

304 equal to $196 \mu\text{mol mol}^{-1}$, a value very close to the average CH_4 concentration inside the hood after 10 min
 305 (which contour is highlighted with the dashed line in Fig. 5a), equal to $208 \mu\text{mol mol}^{-1}$, which can also be
 306 calculated as shown in Eq. 5:

$$307 \quad \bar{c}_{\text{CH}_4} = \frac{\dot{Q}_{\text{LFG}} * \bar{c}_{\text{CH}_4, \text{LFG}} * \Delta t * S_h}{V} \quad (5)$$

308 After the FID operation time of 2 min (Fig. 5b), the system is perturbed with respect to the static
 309 deposition period (Fig. 5a), giving a fairly mixed system. The simulation results show that the CH_4
 310 concentration at the sampling point after this time (10 + 2 min) is $260 \mu\text{mol mol}^{-1}$, compared to an
 311 average CH_4 concentration in the chamber of $248 \mu\text{mol mol}^{-1}$. These results confirm both the
 312 appropriateness of the choice of the sampling point and consequently the legitimacy of the assumption of
 313 considering the CH_4 concentration value measured with the FID at the sampling point as representative of
 314 the average CH_4 concentration inside the hood. A more detailed study of the trend of concentration inside
 315 the hood and the validation of the CFD results with the experimental data has been presented elsewhere
 316 (Lucernoni *et al.*, 2016b).



317

318

Figure 5. CH_4 concentration distribution after 10 min (a) and after 10+2 min (b).

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320

321 *LFG emissions and meteorological parameters*

322 The first step of this part of the work was the selection of the meteorological parameters deemed as the
323 most influential on the LFG emissions. The wind velocity and the wind direction were excluded since the
324 sampling method adopted is a hood isolating the sampling area, making the action of the wind
325 uninfluential, especially for the present study where the source is located in a region characterized by
326 weak winds. Air temperature proved to have a small influence on emissions, probably because the waste
327 decomposition process is in an advanced stage and external air temperature has a minimal influence on
328 the phenomenon. There could be also an alternative explanation: considering that the air temperature only
329 has an influence on soil temperature up to a certain depth (1-2 m below the surface), the temperature in
330 the landfill body is typically constant. As most of the waste is located deeper than that, it is possible that
331 the air temperature will not affect LFG generation.

332 On the other hand, there are some studies in literature investigating the effects of temperature on
333 microbial methane oxidation in landfill cover soils, which might thus have measurable consequences on
334 methane emissions from the landfill surface to the atmosphere (e.g., Börjesson *et al.*, 2004; Einola *et al.*,
335 2007; Spokas & Bogner, 2011). However, most of these studies have been performed on a laboratory-
336 scale or by isolating a portion of the cover soil to be tested, and in general, up to now, there have been
337 very few field studies that have attempted to investigate the relative contribution of the effective temporal
338 dynamics and the relative contribution of such environmental parameters directly on landfill surfaces
339 (Scheutz *et al.*, 2009). For this reason it is very difficult to make accurate and quantitative considerations
340 about the possibility that temperature is negatively correlated to CH₄ emissions from landfill surfaces.
341 Moreover, in those laboratory studies, significant variations of CH₄ emissions were observed only for
342 considerable temperature differences by controlling other parameters. For this study, samples were
343 collected always in the morning, giving that the temperature differences were significant only when
344 comparing measurements carried out in different seasons, and in such a long time frame and with other

345 parameters affecting the CH₄ emissions more than temperature, it is unlikely that such effects of
 346 temperature on the potential of methane oxidation are observed.

347 Air humidity seems to not have a significant influence on LFG emissions, which was hypothesized a
 348 priori since there is no theoretical justification for that and no mention of a possible influence of air
 349 humidity on the emissions was found in literature neither. Up to now, there are no conclusive evidences
 350 that solar radiation directly affects the emissions, even if several undergoing researches are trying to study
 351 a possible cross-correlation between radiation and atmospheric pressure, since both parameters are
 352 indicative of the weather conditions. Rainfalls were not investigated directly as a parameter, it was
 353 preferred to consider the soil humidity. Therefore, the variables considered for the study were
 354 atmospheric pressure and soil humidity. As explained in the scientific literature, it is possible to ascribe
 355 the negative influence of pressure increase on LFG emissions to a phenomenon called landfill
 356 “respiration”: in some cases, a weak negative correlation was found between the two variables. According
 357 to this explanation, a pressure increase “pushes” the biogas into the soil, obstructing the emission. In
 358 order to investigate the effectiveness of this hypothesis, the daily and monthly pressure trends were
 359 analysed as well as the pressure gradients during the 3 and 6 hours preceding each campaign. The only
 360 correlations that were identified are those between emissions and instantaneous pressure at the time of the
 361 sampling, and the average pressure in the preceding 24 hours and 48 hours. The preliminary analysis of
 362 the data shows a correlation that – differently from what has been found in some other studies – is
 363 positive; even though weak, the correlation seems to indicate an increase of the LFG emission with
 364 atmospheric pressure. This observed correlation might be partially explained based on some
 365 considerations found in the manual “Solid Waste Engineering” by Sirini et al. (2010), which in Chapter
 366 15 discusses the migration of trace gases across the landfill surface (Eq. 6).

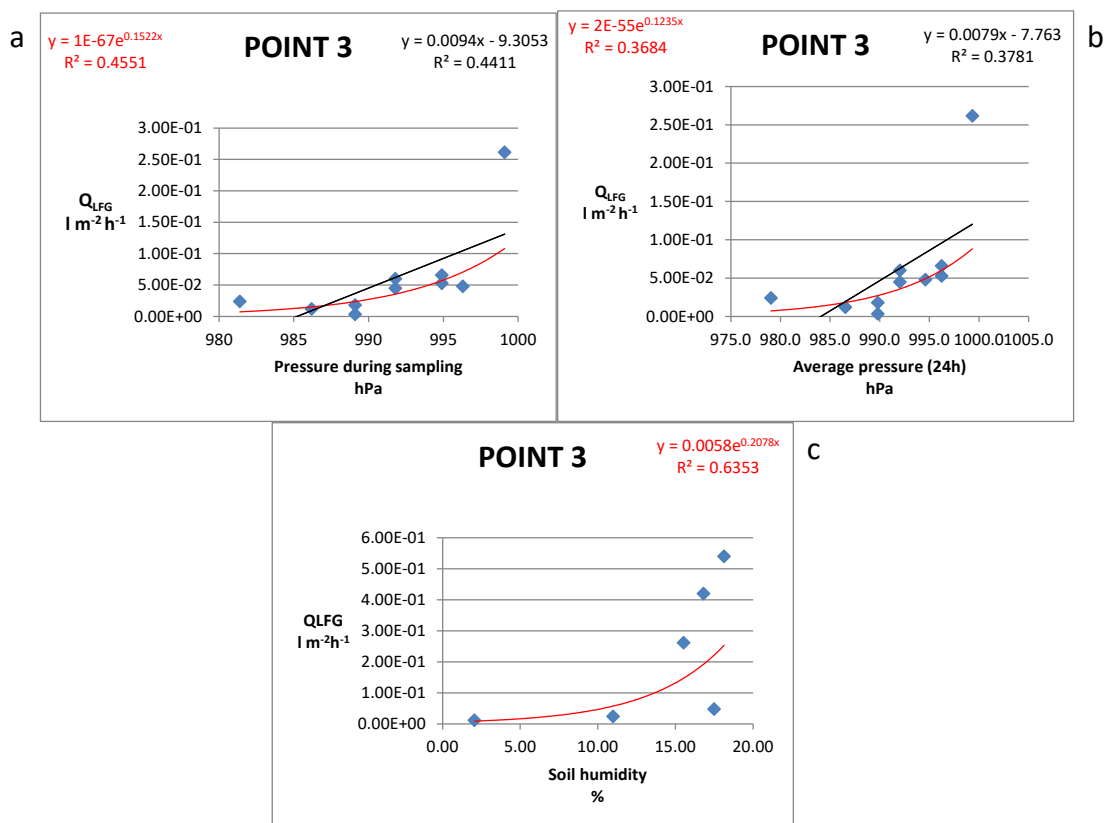
$$367 \quad J_i = \frac{D_i \cdot \alpha^{4/3} \cdot (C_{i,atm} - C_{i,s} \cdot W_i)}{L} \quad (6)$$

368 The authors indicate that the emission flux of the specific gas (J_i) is a function of several parameters, such
 369 as molecular diffusivity (D_i), soil porosity (α), atmospheric gas concentration ($C_{i,atm}$), saturation gas
 370 concentration ($C_{i,s}$), scaling factor (W_i) and landfill covering thickness (L). It is possible to assume that all
 371 the parameters contained in the equation are not affected by atmospheric pressure, except the diffusivity,
 372 which is related to the soil porosity. Therefore, it is possible that, since high pressure indicates a “no-rain
 373 condition”, the soil porosity will be higher and thus emission will be higher as well.

374 As an example, the correlation between specific LFG flow rate and atmospheric pressure (instantaneous
 375 and average of the preceding 24 hours) relevant to sampling point #3 is shown in Fig. 6a and 6b.

376

377



378

379 **Figure 6.** *Landfill gas emission vs. environmental parameters. LFG emission vs. atmospheric pressure at*
380 *the time of sampling (a) and vs. average atmospheric pressure in the 24 h preceding the sampling (b) and*
381 *vs. soil humidity (c).*

382 Concerning the correlation between LFG emissions and soil humidity, a positive correlation was found
383 and the LFG emission seems to increase with the soil humidity (*e.g.* Fig. 6c shows the correlation
384 between LFG emission and soil humidity relevant to sampling point #3). This only is true in the case of
385 no-rain, since during rainfall a sort of “cork” effect is observed due to the obstruction of the pores and
386 thus reduced diffusivity, and measured emissions from the landfill surface are 0. In order to give an
387 explanation to this experimental evidence, some considerations about the operation of the studied landfill
388 should be made. In the examined landfill the common practice of “leachate recirculation” inside the waste
389 mass is not performed, the leachate formed during waste fermentation is compelled by gravity to move
390 downwards, giving that the upper levels of waste will be typically dry and thus generate less biogas due to
391 slower fermentation kinetics. Moreover, given that the closed allotments of the studied landfill are not
392 fully waterproofed, during rainfall, water trickles across the soil wetting those wastes stored in the upper
393 levels, which are normally dry: this might speed up the LFG production kinetics and cause higher
394 emissions. However, there may be an alternative reason as well: the hotspots can be assumed to contain
395 wider pores than the soil around these hotspots. Therefore, if it starts raining the pores in the soil may be
396 obstructed more and earlier than the pores in the hotspot. This may drive a larger portion of the emission
397 through the hotspot without affecting the overall landfill emission.

398 The correlation observed in Fig. 6c looks more exponential than linear. This observation would be
399 coherent with the influence of the humidity found in most expressions for the CH₄ production kinetics via
400 waste fermentation. As an example, the equation used by the US-EPA software LandGEM (Alexander *et*
401 *al.*, 2005) describes an exponential trend whereby the exponent contains the kinetic constant (k), which
402 depends mainly on the soil humidity:

403
$$Q_{CH_4} = \sum_{i=1}^n \sum_{j=0,1}^1 kL_0 \left(\frac{M_i}{10}\right) e^{-kt_{ij}} \quad (7)$$

404 **Conclusions**

405 The first aim of the work was the definition of a reliable and reproducible sampling procedure. The
406 optimal procedure defined is based on the use of a SH, with a static sampling time of 10 min followed by
407 2 min required by the FID for the CH₄ concentration measurement. The CFD simulations confirmed the
408 basic assumptions for the definition of this sampling method: linear CH₄ concentration growth during the
409 established sampling time and equivalence between measured CH₄ concentration and average CH₄
410 concentration inside the hood, as well as the appropriateness of the chosen sampling point.

411 The second aim was a preliminary study of the correlation between LFG emissions and meteorological
412 parameters; the most influential parameters were identified, these being atmospheric pressure and soil
413 humidity. Some preliminary positive correlations were observed between those parameters and the LFG
414 emission from the landfill surface.

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